

LISTING OF CLAIMS

Claims 1-7 (Cancelled)

8. (Amended) Process for the catalytic fluorination of saturated or olefinic halogenated hydrocarbons by HF in the gas phase, comprising fluorination with characterized in that a catalyst based on chromium and on nickel which are obtained by impregnation of an amorphous chromium III oxide with a solution of a nickel derivative, characterized in that the chromium oxide used exhibits a BET specific surface of greater than 150 m²/g and a pore volume of greater than 0.15 ml/g, according to one of Claims 1 to 7 is used.

9. (Amended) Process according to Claim 8, wherein in which, before it is used, the catalyst is dried under an inert gas or under air at a temperature of between 100 and 350°C and then activated with HF.

10. (Amended) Process according to Claim 9, wherein in which the HF is first introduced diluted in air or, optionally preferably, in an inert gas at a temperature ranging from 150 to 200°C and then pure at a temperature of less than 400°C, preferably of between 350 and 380°C.

11. (Amended) Process according to ~~one of Claims~~ Claim 8 to 10, wherein in which the fluorination temperature is between 50 and 500°C, preferably between 100 and 450°C and more particularly between 120 and 400°C.

12. (Amended) Process according to ~~one of Claims~~ Claim 8 to 11, wherein in which the contact time is between 3 and 100 seconds, preferably less than 30 seconds.

13. (Amended) Process according to ~~one of Claims~~ Claim 8 to 12, wherein ~~in which~~ the molar ratio: HF/halogenated hydrocarbon(s) is between 1/1 and 30/1, ~~preferably less than 20/1.~~

14. (Amended) Process according to ~~one of Claims~~ Claim 8 to 12, wherein ~~in which~~ the fluorination is carried out at an absolute pressure of between 0.08 and 2 MPa, ~~preferably between 0.1 and 1.5 MPa.~~

15. (Amended) Process according to ~~one of Claims~~ Claim 8 to 14, wherein ~~in which~~ the fluorination is carried out in the ~~present~~ presence of an oxidizing agent, optionally ~~preferably~~ oxygen or air.

16. (Amended) Process according to ~~one of Claims~~ Claim 8 to 15, wherein ~~in which~~ the catalyst, deactivated by coking, is regenerated by treatment with air or with oxygen or by a Cl₂/HF mixture, at a temperature of between 250 and 400°C.

17. (Amended) Process according to ~~one of Claims~~ Claim 8 to 16, wherein ~~in which~~ the halogenated hydrocarbon is perchloroethylene or 1-chloro-2,2,2-trifluoroethane.

18. (New) Process according to Claim 10, wherein the temperature is between 350 and 380°C.

19. (New) Process according to Claim 11, wherein the temperature is between 100 and 450°C.

20. (New) Process according to Claim 11, wherein the temperature is between 120 and 400°C.

21. (New) Process according to Claim 12, wherein the contact time is less than 30 seconds.

22. (New) Process according to Claim 13, wherein the molar ratio is less than 20/1.

23. (New) Process according to Claim 14, wherein the pressure is between 0.1 and 1.5MPa.